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Flow Rate Controlled Pipetting for Microfluidics: Second Generation Flexible Hydraulic Reservoir (FHRv2)

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Abstract

A critical component of microfluidic technology is the fluid pumping mechanism. Syringe and pressure pumps are typically used in the lab environment, however their operations generate considerable dead volume that is often larger than the volume of the chip itself, leading to considerable waste of precious sample. As an alternative, pipetting allows for precise liquid dispensing with zero dead volume however, it has a limited flow control. Recently, we have introduced a low-cost sample loading interface with zero dead-volume named flexible hydraulic reservoir (FHR). In this study, we present a second generation, FHRv2 that combines continuous pumping, zero-dead volume and the versatility of pipetting. The performance of FHRv2 is tested against a syringe pump at flow rates ranging between 20–60 µL/min. It demonstrated smoother operation and identical transient time to reach steady flow rate as confirmed by a mathematical model developed for the occasion. Importantly, we also demonstrate that the FHRv2 prevents sedimenation-induced artifacts typically encountered in typical syringe pumps when dispensing particles. Finally, we demonstrate the fabrication of the FHRv2 concept with injection molding using a 3D printed mold. Overall, our FHRv2 offers a low-cost and versatile solution for zero-volume liquid handling in microfluidic devices.

Keywords: Zero dead-volume, Precise liquid dispensing, Flow-rate controlled pipetting

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1 Introduction

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Microfluidics has enabled advances in numerous applications including synthesis and analysis of chemicals and 39 biological materials, point-of-care (POC) testing [1], drug delivery, [2, 3] and cell-handling [4, 5] as well as organs-on-a-chip platforms that [6, 7] mimic *in-vivo* environments. Although passive techniques such as capil-41 lary pumping [8] or gravity [9] may sometimes be employed for driving the liquid, long-term, stable delivery of 42 fluids into the microfluidic channel network typically requires a pumping system. In laboratory environment, 43 the most commonly used sources of pumping mechanisms are syringe and pressure pumps. However, these pumps that reply on tubing to connect the microfluidic chips, typically introduce considerable dead volume 45 during operation. To overcome the dependence on bulky external hardware and to minimize the dead vol-46 ume, a number of micro pumps have been proposed. The common desired characteristics of these pumping 47 systems include (i) flow control, (ii) a wide range of flow rates, (iii) an appropriate back pressure and ideally 48 (iv) low-cost. Some micro pumps employ moving mechanical parts, typically an oscillating diaphragm actu-49 ated by a number of mechanisms, including hand power [10, 11], electrostatic [12], electromagnetic [13–16], 50 piezoelectric [17-19], thermo-pneumatic [20] forces or rotary motion of vanes and gears [21]. Even though 51 diaphragms made of soft material are utilized most of the time, [12–19, 22], thermoplastic elastomers were 52 also implemented, which enabled production of the device by common mass production techniques [23, 24]. 53 The micro pumps employing moving mechanical parts require either miniature valves with moving parts or non-moving nozzle/diffusers to rectify the fluid flow. Owing to the oscillating or reciprocating nature of the actuation, a pulsation (i.e. back flow) is present to some extent for these types of pumps. Although valveless 56 design is simpler to fabricate, pulsating flow is even more pronounced due to the lack of active check valve. 57 Another class of micro pumps, which does not rely on any moving parts, employ the interaction of fluid with 58 an external field to induce continuous flow. The external field may be electrical [22, 25] magnetic [26, 27] 59 [28], acoustic [29, 30] or chemical [31]. However, the flexibility of continuous pumps is limited. For example, 60 for electrokinetic pumping, the maximum electric field employed depends on the electrical conductivity of the 61 liquid. This is to avoid the adverse effects of Joule heating, which may not compatible with a number of biological applications [32]. For magnetic actuation, the liquid needs to have specific magnetic properties and/or 63 contain magnetic particles [27]. For acoustic actuation, piezoeletric actautors need to be integrated within the microfluidic device and require relatively complex electronic hardware [29, 33]. 65

Despite the diversity of micro pumps and actuation techniques available, syringe pumps along with pressure pumps have established themselves as the most viable option for microfluidic applications due to their simplicity and robustness [34, 35]. Pressure pumps operate based on the modulation of air pressure in a sample reservoir. Even though pressure pumps provide a stable fluid flow, which may be quite important for some applications such as droplet generation[36], they require expensive connectors, tubing as well as sensors and controllers, which comes at a cost. In addition, an infrastructure for pressurized air supply is also required for their operation. Considering the entire system with all the necessary components, a pressure pump may cost up to \$10,000 [37]. Recently, Thurgood et al. [38, 39] presented a pressure pump using latex balloons attached to syringes which reduce the cost of the system dramatically and makes the pressure pump suitable for low resource settings. However, despite the simple instrumentation, the controlled flow rate requires the monitoring of the pressure inside the ballon, and the balloons occupy a bulky volume compared to the microfluidic device,

especially when several balloons are used.

Syringe pumps rely on the displacement of a piston to deliver the sample from a disposable syringe to a microfluidic device. Commercial syringe pumps are typically delivered with integrated control electronics. They represent a relatively inexpensive solution with an entry price about \$750 [40]. Since the liquid is incompressible, the liquid flow is solely controlled by the displacement of the piston. Although syringe pumps may also induce pulsation, especially at low flow rates, due to the friction between the cylinder of the syringe and the piston. Additionally, flow rate fluctuations may also be experienced due to the oscillations of the motor (depending on the quality of the hardware). However most of the time, these variations are tolerable and do not affect the performance of the operation. Another drawback of syringe pumps is that, especially in applications that require infusion of a cell suspension, cells sediment at the bottom of the syringe barrel during the operation, which hinders homogeneous dispensing. Magnetic stirrer integrated syringe pumps are available [41] or vertical syringe pumps may be used to address this issue.

In many microfluidic applications, rare and/or valuable samples, chemicals and reagents need to be introduced into the microfluidic device. In these situations, delivery of minute amount of valuable samples with minimum dead volume is vital. Although low-cost macro-scale syringes and tubings are easy and convenient to use with syringe and pressure pumps for microfluidic applications, they may create great amount of dead volume. Alternatively, micro-scale capillaries and syringes can be used; however, these components may be too expensive to be used as a disposable set; in addition, integration and sealing may require some special care [42]. As an alternative to syringe and pressure pumps, pipetting is a very convenient and versatile option to precisely control the amount of liquid dispensed with zero dead volume during the operation. However, regular pipettors do not allow control of the flow rate. Recently, Kim et al[43] proposed and described the operation of a pipetting driven microfluidic immunohistochemistry platform. Throughout the process, a pipette was connected to the microfluidic platform with a PDMS adaptor, and the valuable sample in small size was infused into the microchannel. Kim and Choi [44] introduced a "smart pipette" composed of a syringe (which was employed as the actuator), an air chamber and a conventional pipette tip (which was employed as the sample holding container). The volumetric flow rate was adjusted by the variable volume of the syringe; however over the operation of 200 seconds, the flow rate was observed to vary by 15%. Therefore, if the precision on the flow rate does not affect the performance of the device, smart pipette is an excellent solution especially for low resource settings, but the accuracy of control of the flow rate is well below than that of syringe and pressure

Recently, Hatipoglu *et al.* [45, 46] offered a low-cost, disposable sample loading interface named flexible hydraulic reservoir (FHR) which can be an attachment to any syringe available. FHR contains two types of fluids; the dummy fluid and the sample fluid, respectively. Dummy fluid is loaded both into the syringe and the interconnect tubing from the syringe to the FHR. The valuable fluid is loaded on the second compartment, which is isolated from the dummy fluid through an elastic membrane. FHR is connected to a microfluidic device to enable the infusion of all of the valuable liquid, which is deposited on the second compartment, into the microfluidic platform with zero-dead volume. In this previous version of FHR, the valuable liquid must be loaded to avoid air trapped between the membrane and the liquid, such that the valuable liquid can be delivered at a rate equal to that provided via the syringe. However, this requires a rigorous loading process, which is considered as a major drawback of FHR. One other drawback of this system was non-standard means

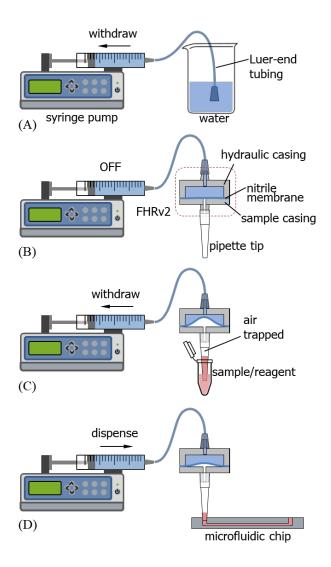


Figure 1: Operating principles of FHRv2

of connection needed to interface the FHR with the microfluidic chip. FHR must be mounted directly onto the inlet of the microfluidic device to ensure zero-dead-volume dispensing of the valuable liquid to the device. These drawbacks seriously reduced the loading and dispensing versatility of the device. Here we address these issues by integrating a pipette tip to the FHRv2, thus enabling a world-to-chip interconnect for versatile sample loading and dispensing. Doing so, we combine flow rate control offered by the syringe pump, the zero dead-volume of FHR, and the versatility of pipetting.

The operating principle of FHRv2 is given in Fig. 1. As seen from the figure, the user does not need to load the sample into the syringe and interconnect tubing. Instead, they are always filled with a dummy fluid, and the user loads the sample into a pipette tip as with a regular pipette. The pipette tip is the only disposable component of the FHRv2. Integration of pipette tip introduces an important aspect of FHRv2, that is compartmentalization of the elastic membrane and the loaded liquid sample through air trapped in the pipette tip. This results in a capacitive behavior that damps out the potential oscillations due to the syringe pump. However, it also induces a time lag between the response of the syringe pump and the FHRv2. To predict the transient behavior of FHRv2 due to capacitive effect of air entrapped in the pipette tip (and the sample casing) during loading of the sample, a mathematical model relating the time dependent flow rate at the outlet of the FHRv2 to the trapped air volume

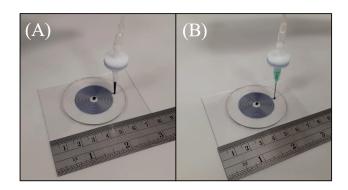


Figure 2: The integration of the FHRv2 to a microfluidic device through (A) a pipette tip and (B) a syringe needle

(which is equal to the internal volume of the pipette tip) and the infusion rate of the syringe pump. Through the mathematical model, developed in MATLAB 2019b Simulink environment, we observed that this lag time 133 is in the order of ten seconds with conventional pipette tips. However, both syringe pumps and FHRv2 reach 134 steady state flow rate at approximately the same time due to a shorter settling time for the FHRv2, as explained 135 below. Besides, the lag time of the FHRv2 can be minimized through the adjustment of the air volume (e.g. by 136 using a syringe needle instead of a pipette tip). The integration of the FHRv2 to a microfluidic device through 137 a pipette tip and a syringe needle is illustrated in Fig. 2. The model compares favorably with experiments 138 during which the displaced volume is obtained by tracking the motion of a fluorescent dye-oil interface with an in-house developed image processing algorithm. We also developed a fabrication scheme as a first step in 140 scalable manufacturing of FHRv2 by injection molding using polymer rapid tooling with a 3D printed mold. 141 Finally, we demonstrated the use of FHRv2 to feature its feasibility in particle-based applications. 142

2 Materials and Methods

144 2.1 Mathematical Model

The mathematical model was built based on hydrodynamic-electrical circuit analogy using MATLAB R2019b Simulink (Fig. 3). The syringe pump was modeled as a current source, the tubing connecting the syringe to the FHRv2 as a resistor, FHRv2 with the pipette tip as a capacitor, and the microchannel as a resistor, accordingly. The resistance of the tubing (R_t) was calculated as:

$$R_t = \frac{128\mu L_t}{\pi D_t^4},\tag{1}$$

where μ is the dynamic viscosity of water, L_t and D_t are the length and the diameter of the tubing, respectively. Similarly, the resistance of a typically rectangular microchannel can be obtained using:

$$R_c = \frac{12\mu L_c}{wh^3 \left(1 - \frac{0.63h}{w}\right)},\tag{2}$$

where L_c is the wetted length of the microchannel, w and h are the width and the height of the microchannel, respectively. On the other hand, since we have utilized sufficently long 0.7 mm ID tubing instead of a microchan-

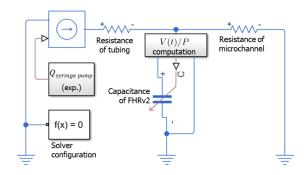


Figure 3: MATLAB Simulink model used for predict the transient response of FHRv2. See ESI for the details of the model.†

nel in flow characterization experiments (Fig. 5A), we used (Eq. (1)) to calculate the hydrodynamic resistance at the downstream of the FHRv2. The capacitance due to compliance of the tubing and the microchannel were 154 neglected, since the major capacitive effect is due to the air trapped shown in Fig. 1C. Moreover, the capaci-155 tive effect of the deformation of the nitrile membrane was ignored as the change in the volume underneath the 156 membrane due to the deformation of the membrane was quite insignificant in comparison to its deflection [45]. The capacitance of air trapped (C_{air}) in the hydraulic circuit is 158

$$C_{air} = \frac{V(t)}{P},\tag{3}$$

where V(t) is the instantaneous volume and P is the absolute pressure of the air trapped, respectively. To calculate the capacitance of air trapped in FHRv2, (Eq. (3)), the instantaneous volume and the absolute pressure need to be determined. To obtain the instantaneous volume of air trapped (V(t)), the integral of the instantaneous current (equivalent to the instantaneous flow rate, Q(t)) passing through the capacitor was subtracted from the 162 initial volume of the air $(V_{air,i})$, since the current basically indicates the rate of the volume of air compressed. Similarly, to obtain the absolute pressure of the air trapped, voltage drop (equivalent to the pressure drop, ΔP) across the capacitor was added to the atmospheric pressure (P_{atm}) . As a result, the capacitance of the air trapped was determined as:

$$C_{air} = \frac{V_{air,i} - \int_0^t Q(t)dt}{\Delta P + P_{atm}}. (4)$$

This computation scheme introduces an algebraic loop in the model, which must be iteratively solved at each time step of the simulation. To ensure the convergence of the solution, initial value of the capacitor was set as: 168

$$C_{air,i} = \frac{V_{air,i}}{P_{atm}}. (5)$$

Fabrication via mechanical machining 2.2

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The hydraulic and sample casings of FHRv2 were fabricated by respectively turning and drilling a cylindrical 170 polyimide stock of 25 mm diameter by using a manual lathe (Opti D320 x 920 lathe, Optimum Machinen, Germany). Inlet of the hydraulic casing and outlet of the sample casing were tapered in accordance with the 172

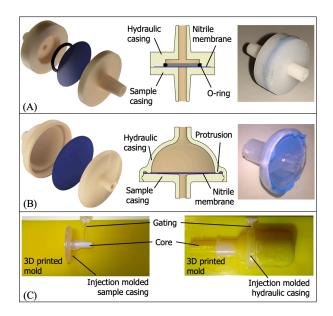


Figure 4: (A) Exploded view, cross-section view of 3D CAD model and photo of assembly of mechanically machined FHRv2, (B) exploded view and cross-section view of 3D CAD model and photo of assembly of injection molded FHRv2, and (C) details of the 3D printed mold for injection molding of hydraulic casing and sample casing of FHRv2. See ESI for the STL files for both mechanically machined and injection molded FHRv2.†

dimensions of standard male Luer-cone connector and the neck of 250 μ L pipette tip. The dimensions of the hydraulic casing were set such that the inner volume was 120 μ L. After machining, an O-ring was placed in the hydraulic casing as an elastic seat for to prevent leakage. Then, the nitrile membrane was slightly stretched flat and bonded to the hydraulic casing by applying epoxy-based adhesive. The sample casing was then adhesively bonded to the nitrile membrane to finalize the assembly. Fig. 4:A shows the exploded view and the cross section view of the CAD model, and the assembly of FHRv2 fabricated by mechanical machining.

2.3 Fabrication via plastic injection with 3D printed mold

The polymer tools for molding the hydraulic casing and the sample casing were printed by using polyjet printer (StrataSYS J750, Stratasys Ltd) due to its high feature size resolution and robustness. We used Vero TM range materials of the printer with gloss finish on the surface, as its low friction coefficient is ideal for part release. Post processing of the tools was undertaken using a jet washer (Genie Pro-600, Gemini Cleaning Systems Ltd) followed by air drying. To define the inner volume and the inlet hole of the hydraulic casing, a 3D printed core has been implemented. In addition, to define the outlet hole of the sample casing, a polymer pin was used as a core. Fig. 4C shows the details of the 3D printed molds and the cores. Once assembled, the mold with the core was fitted to the bolster plate on the injection molding machine (Microsystem 50, Battenfeld). Polypropylene (C711 70RNA, Braskem) was injected into the mold under 200 bar of holding pressure and 190°C nozzle temperature to mold the hydraulic and sample casings.

Following the injection molding, the hydraulic and sample casings with nitrile membrane in between are brought together by using finger pressure until the parts are mechanically locked for assembly. By taking advantage of injection molding and 3D printing, we have revised the design of the FHRv2 such as to make the

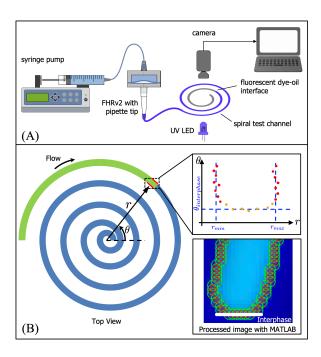


Figure 5: (A) Test set-up used for flow characterization of FHRv2, and (B) illustration of the image processing scheme used to measure the volume dispensed

inner cavity of the hydraulic casing in a dome shape structure, to accommodate the nitrile membrane deformation during intake of the sample (Fig. 2C). We also revised the assembly scheme such that the sample casing could be snap fit into the hydraulic casing, while sandwiching the nitrile membrane in between. Fig. 4B shows the exploded view and the cross section view of the CAD model, and injection molded FHRv2. A protrusion that presses on the nitrile membrane was placed at the bottom of the hydraulic casing to prevent leakage (Fig. 4B).

2.4 Flow Characterization

Fig.5A illustrates the test set-up. with mechanically machined FHRv2 used in the experiments. A sufficiently long spiral test channel was utilized to measure the displaced volume by FHRv2 as a function of time. The test channel was formed by inserting an ID 0.7 mm tubing (the value of the diameter was also verified by microscope measurements) into a spiral shaped groove on a 3D printed template. The test channel was filled with oil prior to testing. Then, 60 μL fluorescent dye was drawn into the pipette tip mounted at the outlet of the sample casing of the FHRv2 and the pipette tip was fitted into the inlet of the test channel, such as to form a fluorescent dye-oil interface. During the test, the dye was injected through the test channel via FHRv2 by running the syringe pump (NE1002X, New Era Pump Systems) in dispense mode. The location of the fluorescent dye-oil interface, which can be related to the volume dispensed, was monitored by a camera (Phantom MIRO LC-110, Adept Turnkey Pty Ltd) at a rate of 30 fps under UV-A illumination to enhance the contrast between the dye and oil. Captured frames were then analyzed by using a custom image processing script written on MATLAB to determine the location of the interface with respect to time. The same experiment was carried out in the absence of FHR, such that the test channel was directly connected to the tip of the syringe, to measure the volume delivered by the syringe pump. Due to uncertainties in locating the interface by image processing and possible non-uniformities of the internal surface of the tubing, fluctuations were observed in the measured volume at 30 fps capturing

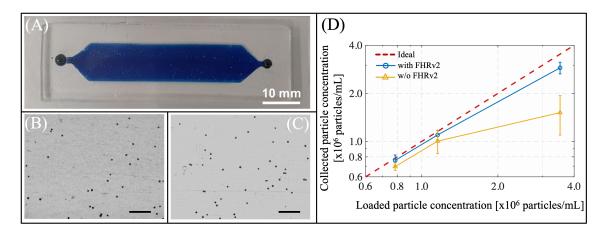


Figure 6: (A) Test chip used for particle dispensing experiments. Sample frames captured during particle dispensing (B) without FHRv2 and with (C) FHRv2. Loaded particle concentration is 0.76×10^6 , scale bar indicates 200 μ m. (D) Collected particle concentration versus loaded particle concentration at $Q = 40 \,\mu$ L/min. Dash line indicates the reference.

frequency. The data was decimated by 20 to eliminate the noise, while preserving the trend.

Total volume dispensed was determined by processing the data obtained from the camera. The image processing was performed to measure the distance covered by the interphase between fluorescent dye and oil in the test channel at each frame, and then summing up the incremental distances over frames. In this process, firstly the frames were converted to binary images. Then, the coordinates of the boundary of the interphase were determined by means of built-in MATLAB function by boundaries. Once the coordinates of the interphase was determined, the angular (θ) and the radial (R) coordinates of each pixel in the vicinity of the interphase with respect to the center of the spiral (as the center of the coordinate frame) were computed to generate a plot of θ vs. r, as shown Fig.5B. Based on this data, a mean angle $\bar{\theta}$ and a mean radius $\bar{r} = (r_{min} + r_{max})/2$ were computed. At each frame, the pixel with the minimum θ was found and the neighbor of this point (indicated by yellow circles in Fig.5B) which has a θ coordinate within a defined tolerance is included in the calculation of the mean angle as $\theta_{interphase}$. The uncertainty of θ and r coordinates of each point is determined by assigning ± 1 pixel in the normal and tangential directions. Having computed $\bar{\theta}$ and \bar{r} and the associated uncertainty values, the differential distance covered by the interface in each frame was computed, which was related to instantaneous change of the volume dispensed. With the assumption of constant cross-sectional area of the tubing, sum of instantaneous change of the volume yielded volume dispensed up to frame j, (V_j):

$$V_{j} = \sum_{i=1}^{j} (\bar{\theta}_{i} - \bar{\theta}_{i-1}) \, \bar{r}_{i} \, (\pi/4) D_{t}^{2}. \tag{6}$$

The uncertainty in the volume dispensed (ΔV_j) was calculated by using the uncertainty associated with the measurement of the mean angular and radial positions, $\bar{\theta}_i$, $\bar{\theta}_{i-1}$ and \bar{r}_i as:

$$\Delta V_{j} = \sqrt{\sum_{i=1}^{j} \left[\left(\frac{\partial V_{j}}{\partial \bar{\theta}_{i}} \Delta \bar{\theta}_{i} \right)^{2} + \left(\frac{\partial V_{j}}{\partial \bar{\theta}_{i-1}} \Delta \bar{\theta}_{i-1} \right)^{2} + \left(\frac{\partial V_{j}}{\partial \bar{r}_{i}} \Delta \bar{r}_{i} \right)^{2} \right]}.$$
 (7)

232 2.5 Particle Dispensing Experiments

A custom PDMS microfluidic chip was fabricated for particle dispensing experiments as shown in Fig. 6. 233 Total volume of the chip was approximately 20 µL with 50 µm channel height. 13 µm fluorescent particles 234 with known concentrations were dispensed into the chip using a syringe pump with and without FHRv2. To 235 measure the concentration of the loaded particles, 25 µL samples were taken from the prepared suspension 236 loaded onto a hemacytometer and the particles were counted. To measure the concentration of the particles 237 dispensed into the chip, a known region of interest on the chip was recorded at 30 fps during the flow. Captured 238 frames (total of 800 frames per each experiment) were decimated by 20, resulting in 40 frames to be processed. 239 Built-in MATLAB function byboundaries was utilized to locate the particles in the frames (see Fig. 6B 240 and C). Identified particles were counted and the particle count was divided by the volume of liquid in the 241 region of interest to calculate the particle concentration in each processed frame. Average of the processed 242 frames was identified as the collected particle concentration as shown on Fig. 6D. The standard deviation of the concentration among the processed frames was used to define the error bars on Fig. 6D. 244

3 Results and Discussion

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To characterize the flow response of FHRv2, we measured the volume dispensed by FHRv2 at different volumetric flow rates and compared the results with a bare syringe pump. The results for three different volumetric 247 flow rate values ($Q = 20,40,60 \,\mu\text{L/min}$) are displayed in Fig. 7. As seen from the figure, the syringe pump and 248 FHRv2 curves becomes linear and parallel to each other after a transient period. FHRv2 has a longer transient 249 response for all three cases, due to the capacitive behavior induced by the trapped air. The results of MATLAB 250 Simulink model for the FHRv2 with 250 µL pipette tip are also presented in the figure. To compare the exper-251 imental results and the mathematical model, time derivative of the volume delivered by the syringe pump was 252 input to Simulink model. With this approach, an excellent agreement is observed between the experimental data and the model. Therefore, once a user characterizes the syringe pump at hand, the performance of the 254 FHRv2 can be predicted for a given set of operating parameters. 255

To demonstrate the effect of the air trapped on the performance of FHRv2, two cases; 1.5" long 18G blunt needle with ID 0.84 mm (corresponding to 45 μ L inner volume including the Luer hub) and 250 μ L pipette tip were simulated. The experimental flow rate together with the simulated flow rate are given as a function of time in Fig. 8. 10% envelope around the steady-state flow rate value is also shown on the figure (dotted line). All the curves show similar time-dependent behavior, with a rise time (t_r) followed by a settling time (the instant when the response fall within the envelope) before reaching the target flow rate within the envelope. However due to the capacitive behavior of the air trapped, several observations can be deduced:

- The rise time for the FHRv2 is longer than that of the syringe pump, and the rise time increases with increasing air volume.
- The settling time is longer for the syringe pump, and it decreases with increasing air volume.
- The oscillations damp out with the increased air volume both in the transient regime and at steady-state. Especially for the case with larger air volume, the flow rate reaches the steady-state value with a relatively

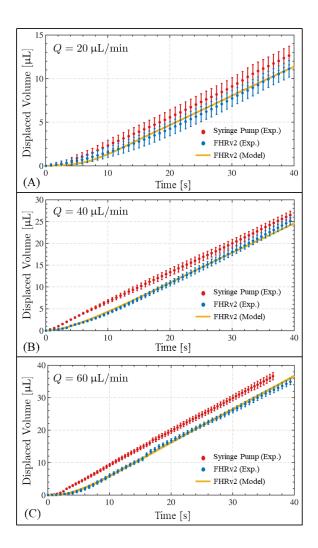


Figure 7: Displaced volume as a function of time: (A) $Q = 20 \,\mu\text{L/min}$, (B) $Q = 40 \,\mu\text{L/min}$, (C) $Q = 60 \,\mu\text{L/min}$

shorter settling period.

Although rise time increases with the introduction of the FHRv2, the settling period decreases compared to the syringe pump. Therefore, the overall transient time for the syringe pump and FHRv2 is similar (<20 seconds for all cases). This result confirms that the capacitive behavior of FHRv2 will not negatively impact microfluidic applications that currently rely on syringe pumps. Additionally, the oscillations observed in the data are due to the syringe pump and are expected to improve with better pumps, which would result in even smoother FHRv2 response.

In addition to flow characterization, we demonstrated the functionality of FHRv2 to prevent non-homogeneous particle dispensing due to sedimentation in typical syringe pumps. For this purpose, we dispensed fluorescent particles at $Q = 40 \,\mu\text{L/min}$ flow rate into a custom test chip by using a syringe pump (Fig. 6A) and a FHRv2 connected to a syringe pump. Fig. 6D reveals that concentration of collected particles is considerably smaller than the loaded concentration when using the syringe pump indicating that significant amount of particles sediment at the syringe barrel. A reduction of $\sim 50\%$ is observed for a particle concentration of $\sim 3.5 \times 10^6$ particles/mL. In comparison, the concentration of the collected particles is much closer to the loaded particles concentration when using the FHRv2. FHRv2 is advantageous in particle dispensing applications as sedimen-

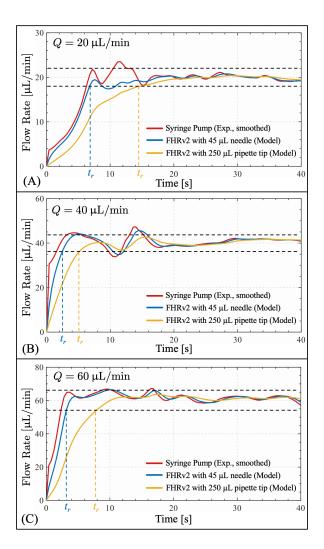


Figure 8: Simulated flow rate as a function of time: (A) $Q = 20 \,\mu\text{L/min}$, (B) $Q = 40 \,\mu\text{L/min}$, (C) $Q = 60 \,\mu\text{L/min}$

tation problem is intrinsically eliminated due to default vertical orientation of FHRv2. However we observed a considerable particle loss ($\sim 10\%$) in relatively higher concentrations of particles ($\sim 3.5 \times 10^6$ particles/mL) (Fig. 6D). Noting that the particles were only contained in the pipette tip and did not interact with FHRv2, we concluded that the loss cannot be related to the geometry or construction of FHRv2. Therefore, this loss is mainly attributed to the errors in experimental procedure.

FHRv2 characterized in flow experiments (Fig. 7) were fabricated by mechanical machining (Fig. 4A), which is typically preferred as an early stage prototyping method [47]. However, some applications including any dispensing of clinical samples may require a single use FHRv2. In such cases, a scalable manufacturing method should be adopted to allow higher fabrication volume. For this purpose, we have developed an injection molding-based manufacturing scheme that utilized 3D printed polymer tools. This approach represents an intermediate step to a scalable alternative.

Injection molding is commonly accepted as the "gold standard" for the fabrication of high volume, low unit cost polymer devices [47]. On the other hand, high cost of steel tooling is not justified in prototyping or low to medium volume production. Polymer additive rapid tooling that reduces the costs in injection molding was first proposed nearly 20 years ago [48], but it only received considerable interest in recent years due to

the democratization of 3D printing [49, 50]. However, very little has been done for geometrically complex, precision micro devices. Here, we demonstrate the use of 3D printed tools in injection molding to manufacture FHRv2 (Fig. 4B,C). We show that despite the low cost of the polymer tool, we were able to maintain feature quality as illustrated in Fig. 4B. We tested injection molded FHRv2 against leakage by applying pressure at the inlet of the hydraulic casing and showed that injection molded FHRv2 could withstand a pressure of 0.4 bars without leakage.

4 Conclusions

A second generation FHR that combines continuous pumping, zero-dead volume and the versatility of pipetting 305 is developed. The performance of FHRv2 is demonstrated in comparison with a syringe pump at flow rates 306 ranging between 20-60 µL/min. FHRv2 provides smoother operation and identical transient time to reach 307 steady flow rate as confirmed by the mathematical model. In addition, FHRv2 prevents sedimenation-induced 308 artifacts typically encountered in typical syringe pumps when dispensing particles. The fabrication of the 309 FHRv2 with injection molding using a 3D printed mold is also demonstrated. Considering all the aspects, FHRv2 is very user-friendly and has a flexible design. It can be implemented with any syringe pump, which is available in almost every microfluidics research environment. It can also be introduced as a very inexpensive 312 set (especially fabricated by injection molding) in a commercial microfluidic product to serve as an interface 313 between the fluid pumping equipment and microfluidic chip. Additionally, since FHRv2 is inherently mounted 314 on a microfluidic chip in vertical orientation, it enables homogeneous delivery of suspension in case of particle 315 or cell based applications. The design of FHRv2 is quite flexible and can easily be modified, and through the 316 mathematical model, the response of FHRv2 can be predicted for a specific application. Our FHRv2 open up new opportunities in low-cost sample handling in microfluidic devices. Its zero dead volume and smooth 318 operation make it particularly suited for handling small amount of precious fluids. 319

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Authorship Contributions

All authors contributed the writing and editing of the manuscript. B.Ç. and E.Y. conceived the idea and developed the mathematical model. A.A., A.T. and B.S. designed the experimental setup and conducted the experiments. B.Ç. and A.A. performed image processing. Mechanical machining of the FHRv2 was performed by E.Y. 3D printing of the mold and injection molding of the FHRv2 was carried out by J.C. and K.C.

Conflicts of interest

There are no conflicts to declare.

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