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Selective electroreduction of CO₂ and CO to C₂H₄ by synergistically tuning nanocavities and surface charge of copper oxide

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KEYWORDS: CO₂ reduction; CO reduction; Electrocatalysis; C₂H₄

ABSTRACT: Electroreduction of CO_2 and CO to high-value chemicals and fuels continues to be a grand challenge. Here we report synergistic electrolysis of CO_2 and CO to C_2H_4 by concurrently tuning nanocavities and the interface of CuO with a hydrogen evolution inactive metal oxide (ZrO_2) . The designed $CuO@ZrO_2$ delivers a faradaic efficiency (FE) as high as $54.7 \pm 1.1\%$ towards C_2H_4 formation and a remarkable overall CO_2 reduction FE exceeding 84.0% at 250 mA cm⁻², significantly outperforming pristine CuO and many recently demonstrated Cu-based catalysts. The composite also exhibits a markedly enhanced FE of converting CO to C_2H_4 , approximately three-fold that of pure CuO. Operando Raman spectroscopy as well as post-mortem XPS measurements verify that Cu^+ species are well retained in the presence of ZrO_2 during CO_2 reduction, in stark contrast to rapid transformation of Cu^+ to Cu^0 in the catalyst without the metal

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oxide. Experiments in combination with theoretical calculations further show that the incorporation of ZrO₂ substantially decreases the dimerization barriers of adsorbed CO intermediates, thus boosting C–C coupling to produce C₂H₄.

INTRODUCTION

The levels of atmospheric CO₂ continue to increase reaching 418.2 ppm (parts per million) in January 2022. This means irreversible and disruptive consequences to our climate and environment. Electrochemical CO₂ reduction (ECR) to fuels or commodity chemicals driven by renewably generated electricity offers a potential strategy to ameliorate greenhouse effect, enabling carbon fixation and energy storage for intermittent renewables. 1-10 Among different products, ethylene (C₂H₄) is an industrial feedstock (for polyethylene) that is in high demand. It is also widely utilized in agriculture to accelerate fruit ripening.⁵ However, it remains challenging to attain efficient ECR to C₂H₄ due to 1) the competitive undesirable H₂O (or proton) reduction reaction; 2) the high energy of the C–C bond and the competitive formation of C-H, C-O, and C-C bonding; and 3) the large overpotential difference between the generation of essential CO species and that of the C₂ moieties. ¹¹⁻¹³ To facilitate the preferential transformation of CO₂ to C₂H₄, prior reports have focused on modification of Cu catalysts through heteroatom alloying, ¹⁶ doping, ^{14,15} or manipulation of facets, ¹⁷ oxidation state, ¹⁸ and surface structure.¹⁹ However, C₂H₄ production via ECR still suffers from low efficiency and selectivity. To circumvent these issues, the preparation and tailoring of synergistic catalytic materials that enable both inhibition of the unwanted hydrogen evolution reaction (HER) and enhancement of CO₂ activation and C-C coupling is highly desirable.^{20,21}

The exact reaction mechanism for C₂H₄ formation from ECR is still under debate. Three major protocols have been put forth: 1) "carbene" mechanism; 2) *CO dimerization (* denotes the adsorbed intermediate); and 3) coupling of CHO* (with *CO or CHO*). 13,22 For the carbine mechanism, hydroxycarbene or carbons are generated and then reduced to *CH₂ species. Further reaction of two *CH₂ moieties or insertion of CO in *CH₂ following a Fischer Tropsch-type manner gives rise to C₂H₄. Alternatively, C₂H₄ can be formed through dimerization of *CO intermediates, which is proposed to be a critical step for C-C bond formation at low overpotentials.²² Two *CO species couple to yield *C₂O₂ which is consecutively hydrated to *CO-COH. Vinyl alcohol (*CH2-CHO) is then formed and further transformed into C₂H₄. Under high overpotentials *CO is predicted to first reduce to *CHO, then subsequently couple with *CO to generate *COCHO, being more preferable than *CO dimerization and reduction. ²² C₂H₄ is obtained via the subsequent formation and reduction of *COCHOH. In an alternative pathway, two CHO* species couple to form OHC-CHO* which converts to *CH₂CHO and is further reduced to ethylene oxide (CH₂CH₂O*). C₂H₄ can then be produced either through direct breaking of C–O bond in CH₂CH₂O* or via hydrogenation to CH₃CH₂OH*.

Regardless of the operational mechanism, *CO is the common intermediate for the production of C₂H₄ and other C₂₊ products. From this scenario, optimizing the coverage and coupling of the *CO intermediate and simultaneously inhibiting undesirable H adsorption are key to boosting CO₂ (and CO) reduction selectively to C₂H₄. In addition, Cu⁺ is supposed to strengthen *CO adsorption (because of the availability of vacant 3d orbitals) to further boost C–C coupling by lowering the Gibbs free energy for *OCCOH formation. Nevertheless, Cu⁺ moieties tend to be reduced under ECR environment, ¹³ resulting in metallic Cu that may

deteriorate the C₂₊ formation. Under such circumstance, stabilization of Cu⁺ species during CO₂ reduction is key. In this work, we seek to explore a synergistic effect by introducing nanoholes and tailoring the interface between CuO and a second component. The porosity of the catalyst favours diffusion of CO₂ to copper sites, thereby significantly increasing the availability of each catalytic center. ZrO₂ is selected as the second phase to create an intimate interface by virtue of its low cost, high surface basicity and good CO₂ adsorption capacity, and outstanding thermal and chemical stability. Meanwhile, ZrO₂ can mitigate the HER.²³ In addition to these benefits, we find that incorporation of the reducible metal oxide can stabilize Cu⁺, as validated by operando Raman spectroscopy, X-ray photoelectron spectroscopy (XPS), and further Bader charge analysis. Such a strategy allows us to readily regulate *CO availability on copper sites, enabling high selectivity to C₂H₄ at large production rates. The ZrO₂ promoted Cu surfaces deliver an FE close to 48% and a cathodic energy efficiency (EE) of ~26.8% towards C₂H₄ formation in an H-type cell. This represents a substantial improvement, outperforming each component alone and many recently reported electrocatalysts. Furthermore, the overall FE and FE for C₂H₄ can be further improved up to $84.3 \pm 1.6\%$ and $54.7 \pm 1.1\%$, respectively under a high current density of 250 mA cm⁻² using a flow reactor. The role of ZrO₂ was also investigated by density functional theory (DFT) modeling, which illustrated a substantially boosted C-C coupling of *CO, thus accelerating C₂H₄ formation.

RESULTS AND DISCUSSION

A facile wet chemical synthesis scheme was used here to fabricate CuO@ZrO₂ composites with adjustable composition. X-ray diffraction patterns (XRD) measurements confirmed the

yield of highly crystalline CuO and ZrO₂. Those diffraction peaks at ~23.9, 28, 31.3, 34, 40.5, 45.3, and 49° can be well assigned to the (011), ($\bar{1}11$), (111), (002), ($\bar{2}11$), (202), and (220) reflections of monoclinic ZrO₂ (JCPDS no.: 74–0815) respectively, while the peaks at around 35.5, 38.7, 48.7, 61.5, and 68° correspond to the ($\bar{1}11$), (111), ($\bar{2}02$), ($\bar{1}13$), and (220) planes of monoclinic CuO (JCPDS no.: 80–1916) (Fig. 1a and Fig. S1). Note that no typical peaks ascribed to reflections of CuZrO₃ (JCPDS no.: 43–0953) were discernible, thus ruling out the formation of the mixed metal oxide.

XPS analysis was performed to probe the chemical composition of the surface and subsurface (up to a depth of 5 nm) of the samples. The wide-survey XPS spectrum reveals the spectroscopic characters of Cu, O, and Zr (Fig. S2a). No other heteroelements including element Cl were detected, indicating the absence of impurities, unreacted precursors or byproducts in the sample. Shown in Fig. 1b are the Cu 2p XPS spectra of pristine CuO and CuO@ZrO₂. The Cu 2p peaks of CuO@ZrO₂ were observed to shift to smaller electron binding energies (BEs) relative to bare CuO, which signifies that the electron charge density around Cu became richer after introduction of ZrO₂. A spin-orbit split doublet with Cu 2p_{1/2} at 953.7 eV and 2p_{3/2} at 933.8 eV for both CuO and CuO@ZrO₂ mainly originates from Cu²⁺ species.²⁴ Three characteristic Cu²⁺ satellites at 961.5, 943, and 940.6 eV were also seen. The deconvoluted Cu $2p_{1/2}$ at 951.9 eV and $2p_{3/2}$ at 932.2 eV suggest the presence Cu⁺ moieties.²⁵ The LMM Auger excitation spectra of Cu (Fig. 1c) confirmed the existence of Cu⁺ in CuO@ZrO₂ which is however not the case for pristine CuO. The intense peak at 568.5 eV can be unambiguously assigned to Cu²⁺, while the Auger peak at ~570 eV arises from Cu⁺. The peak at 574.5 eV represents distinct Auger transitions associated with Cu⁺. ¹⁷ No apparent Cu⁰ signal, supposed at ~568 eV, was identified. The O 1s spectra can be deconvoluted into three sub-bands (Fig. S2b). The signal at about 533.1 eV stems from the surface –OH groups.²⁶ The other two oxygen peaks at ~530.5 and 529.5 eV arise respectively from vacancy oxygen and lattice oxygen.^{14,27} The vacancy oxygen-to-lattice oxygen ratio in CuO@ZrO₂ approximates about 0.58, considerably exceeding the value of ~0.21 for neat CuO and ~0.19 for pure ZrO₂. The increase in oxygen vacancy sites tends to assist in CO₂ adsorption and activation. The two strong peaks with BEs at 181.6 and 184.0 eV are associated with Zr 3d_{3/2} and 3d_{5/2} of Zr⁴⁺ in the composite (Fig. S2c).²⁸ The BE value of Zr 3d_{5/2} was found to be about 0.3 eV higher than that of bare ZrO₂, demonstrating electron transfer from Zr to Cu, in agreement with the result observed for Cu.

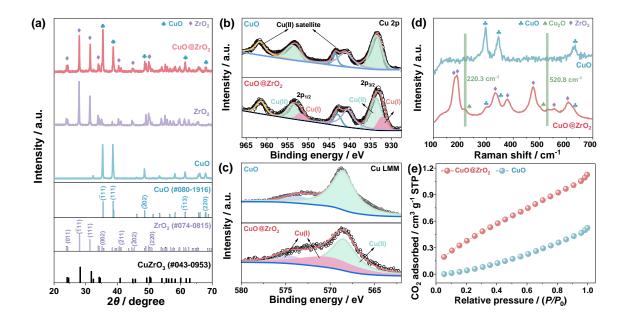


Fig. 1. (a) XRD patterns of CuO, ZrO₂, and CuO@ZrO₂. (b) Cu 2p and (c) Cu LMM Auger XPS spectra, (d) Raman spectra, and (e) CO₂ desorption isotherms of CuO and CuO@ZrO₂.

Raman spectroscopy was employed to probe the local atomic structures and vibrations of CuO@ZrO₂. The signals at 189, 476, and 562 cm⁻¹ can be attributed to the A_g modes while the peaks at 322, 380, and 608 cm⁻¹ are associated with the B_g modes of monoclinic ZrO₂

(Fig. 1d)²⁹. Another distinct peak at 179 cm⁻¹ is likely the $A_g + B_g$ mode of ZrO_2 . Three one-phonon vibrations at 290.6, 345.2, and 626.7 cm⁻¹ were observed for both pure CuO and CuO@ ZrO_2 , corresponding to the A_g mode and two B_g optical modes of cupric oxide.¹⁴ Moreover, two additional peaks at ~220.3 and 520.8 cm⁻¹ were discernible for CuO@ ZrO_2 that can be ascribed to the Cu⁺ species in the composite,¹⁸ in accord with the aforementioned XPS results.

Temperature-programmed reduction by hydrogen (H₂-TPR) measurements present two major peaks at ~200 and 325 °C (Fig. S3), which are associated with the respective stepwise reduction of Cu²⁺ to Cu⁺ and Cu⁺ to Cu⁰ by removing reducible oxygen from the CuO_x species in CuO@ZrO₂. Note that the reduction temperatures obviously decreased compared to pure CuO, which may result from H₂ spillover to CuO at the CuO@ZrO₂ interface. This suggests that adjacent ZrO₂ can help reduce CuO_x in the composite. Equally importantly, CuO@ZrO₂ possesses a CO₂ uptake of ~2.2 mg_{CO2} g_{cat.}⁻¹ at 1 atmospheric pressure and 298.15 K (Fig. 1e), 2.2 fold as large as that of bare CuO, which is mostly attributed to the high CO₂ adsorption capacity of ZrO₂ via carbonate formation. This undoubtedly favours enrichment of CO₂ on the local surface of the cathode and potentially promotes catalytic turnover.

To decipher the morphology and microstructure of the as-made materials, scanning electron microscopy (SEM), transmission electron microscopy (TEM) and high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) were adopted. Despite of the varied Cu/Zr ratios, CuO@ZrO2 catalysts display a capsule-like shape with lateral sizes of ~500 nm (Figs. 2a and b, and S4). Energy-dispersive X-ray spectroscopy (EDS) elemental mapping (Fig. 2c-f), with the corresponding spectrum (Fig. 2g), demonstrated the prevalence and uniform dispersion of Zr, Cu, and O elements throughout the sample, pointing to the

intimate contact between the two metal oxides. Interestingly, several pits on the surface of CuO@ZrO₂ were vividly observed by STEM (Fig. 2h and i, Fig. S5a and b). Higher magnification HAADF-STEM images (Fig. S5a, false color Fig. S5b) reveal that some pits are less than 5 nm in diameter, and are more clearly resolvable at the thinner edges of the capsule. High-resolution TEM observation (Fig. 2j) along with fast Fourier transformation (FFT) (Fig. 2k and l) indicates good crystallinity of the CuO@ZrO₂. Ordered lattice fringes with an interplanar spacing of ~3.2 and 2.7 Å are clearly seen corresponding to the (111), (1 10) planes of ZrO₂ and CuO.³⁰

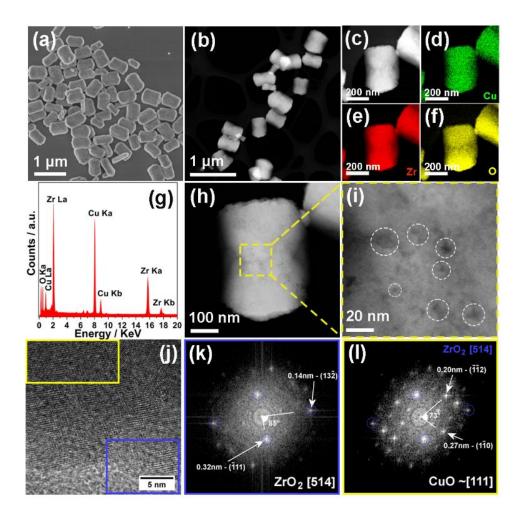


Fig. 2. (a) SEM and (b) low-magnification STEM images, and (c) STEM image and corresponding EDS elemental maps of (d) Cu, (e) Zr, (f) O, and (g) EDS spectrum of CuO@ZrO₂. (h and i) HAADF-STEM images. (j) High-resolution TEM image of CuO@ZrO₂. (k) and (l) FFTs of the areas encased by the blue and yellow rectangles in (j), respectively.

The intrinsic catalytic properties of the as-obtained CuO@ZrO₂ were evaluated for ECR in an air-tight H-type cell with two cathodic and anodic compartments which are separated by using a Nafion 117 membrane with continuous CO₂ flow.³¹ All voltages applied are referred to the reversible hydrogen electrode (RHE) reference unless specified otherwise. Larger reduction current densities were achieved under a CO₂ environment than in an Ar atmosphere across the potential regions (Fig. 3a). At voltages being more negative than –0.6 V, the reduction current increases abruptly in CO₂-saturated 0.1 M KHCO₃ solution, possibly resulting from the occurrence of intense CO₂ reduction. The gas and liquid products were quantified by gas chromatography (GC) and proton nuclear magnetic resonance (¹H NMR), respectively.³²

CO, H₂, HCOOH, CH₄, and C₂H₄ were produced between -0.8 to -1.3 V over both CuO and CuO@ZrO₂ catalysts, whereas only minor amounts of HCOOH were attained on ZrO₂ (Fig. 3b). CO and HCOOH comprise the major ECR products at potentials ≥ -0.8 V. With increase of overpotential, more CO was produced leading to higher *CO coverage. C₂H₄ was preferentially generated at potentials below -1.0 V. The overall ECR FE and the FE for C₂H₄ formation show a volcano-type relationship with the increase of overpotential, reaching a maximum at -1.1 V. Note that both metrics are invariably higher for CuO@ZrO₂ than those on pure CuO in the entire potential range. This underscores the role of ZrO₂ in impeding HER and also promoting the further conversion of adsorbed *CO to C₂H₄ and *CO protonation to

CH₄ (at more negative potentials). Especially, the CuO@ZrO₂ imparts an average maximum ECR FE of 68% and a C₂H₄ FE of 47.6%, approximately 2.1 and 2.4 times that of pure CuO, respectively. Likewise, the highest partial C₂H₄ geometric current density and C₂H₄ production rate of CuO@ZrO₂ are ~5.4 mA cm⁻² and 13.9 μmol mg_{cat.}⁻¹ h⁻¹, 2.3 and 2.5 fold that of individual CuO (Fig. 3c, d and Fig. S6). The partial C₂H₄ current density of CuO@ZrO₂ normalized based on electrochemical active surface area (ECSA) as reflected by double-layer capacitance (*C*_{dl}) (Fig. S7) is 2.3 times that of pure CuO. In addition, the selectivity of ECR to C₂H₄ (FE_{C2H4}/FE_{total}) on CuO@ZrO₂ is much greater than that on bare CuO over a wide potential window from -0.8 to -1.2 V (Fig. 3e). Evidently, the partial current density arising from HER is appreciably lessened after incorporation of ZrO₂ (Fig. 3f).

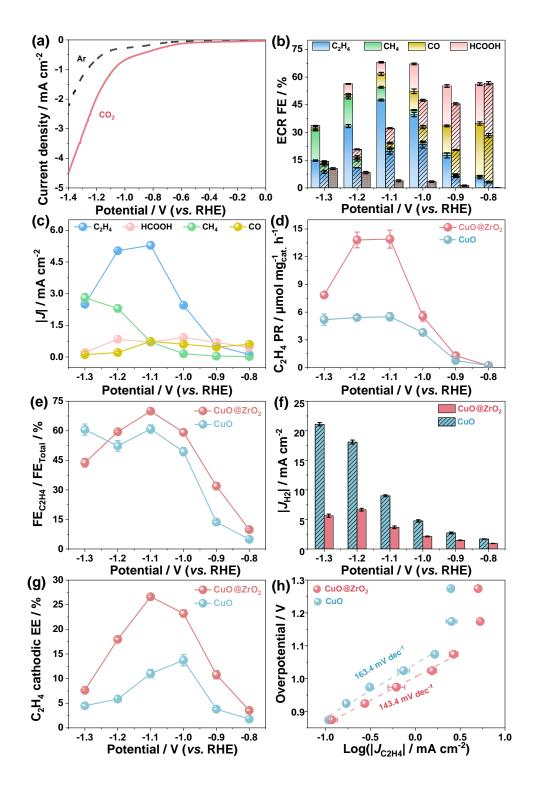


Fig. 3. (a) Linear sweep voltammetry (LSV) curves of CuO@ZrO₂ in 0.1 M KHCO₃ solution saturated with Ar (dashed line) or CO₂ (solid line). The sweep rate is 5 mV s⁻¹. (b) ECR FE over bare CuO (striped column), ZrO₂ (dotted column), and CuO@ZrO₂. (c) Partial geometric current

density for different ECR products over CuO@ZrO₂. (d) C₂H₄ production rate, (e) FE_{C2H4}/FE_{total} ratio, (f) partial geometric current density for H₂ evolution, and (g) C₂H₄ cathodic EE on CuO and CuO@ZrO₂ at various applied voltages. (h) Tafel plots for C₂H₄ production together with corresponding fitting profiles over neat CuO and CuO@ZrO₂.

Furthermore, we calculated the C_2H_4 cathodic EE from the FE for C_2H_4 formation and the ratio of the reaction thermodynamics over cell voltage: [EE = FE_{C2H4} × (E^0 _{O2/H2O} – E^0 _{CO2/C2H4}) / (E^0 _{O2/H2O} – E^0 _{CO2/C2H4} + η _{cathodic})] (Eq. 1). The highest C_2H_4 cathodic EE (26.8 ± 0.3%) was accomplished at 11.2 mA cm⁻² (Fig. 3g). Remarkably, the FE of C_2H_4 on $CuO@ZrO_2$ even exceeds many recently reported Cu-based materials under comparable or larger overpotentials (Table S1), such as the state-of-the-art porous Cu (maximum C_2H_4 FE: 35.8%),³³ Ag₁–Cu_{1.1} nanodimers (maximum C_2H_4 FE: 40%),³⁴ and Cu/GDL (maximum C_2H_4 FE: 40.2%)³⁵. The C_2H_4 EE of 26.8% at 11.2 mA cm⁻² also surpasses most previous results shown over Cu-based electrodes, as summarized in Table S1. Electrochemical impedance spectroscopy (EIS) measurements (Fig. S8) showed a slightly lower charge transfer resistance of CuO@ZrO₂ compared with pure CuO. This enables more facile electron exchange between the working electrode and reactants in the electrolyte, benefiting the ECR. Moreover, a Tafel slope of 143.4 mV dec⁻¹ was observed for CuO@ZrO₂, lower than 163.4 mV dec⁻¹ for pure CuO (Fig. 3h). This indicates that the composite has a relatively faster reaction kinetics for ECR.

The ECR performance could be readily tailored by manipulation of the ratio of the two metal oxides. Increasing the content of ZrO₂ was observed to lead to a monotonic drop of CO FE (Fig. S9). This may be owing to the increased *CO coverage and transformation induced by the incorporation of ZrO₂. Both the overall ECR FE and C₂H₄ FE increased upon improving the Zr/Cu molar ratio, reaching a peak value at the optimal dosage of 2:3 (Fig. 4).

Nonetheless, further increase of Zr content resulted in deterioration of the ECR performance. This is probably due to the reduction in both electrical conductivity and the number of Cu active sites for CO₂ activation. We also found that control of defects (e.g. pits) in CuO by regulating the additional amount of NaOH permits tuning of ECR activity. The overall ECR FE can be greatly augmented to about 68% for defective CuO@ZrO₂, in contrast to that of 18.5% for a counterpart without defects (Fig. S9d). It is noteworthy that under equivalent electrochemical conditions, the overall ECR FE as well as C₂H₄ selectivity over CuO@ZrO₂ are also dramatically superior than those of the commercial Cu, CuO, Cu₂O, and Cu(OH)₂ (Fig. 4).

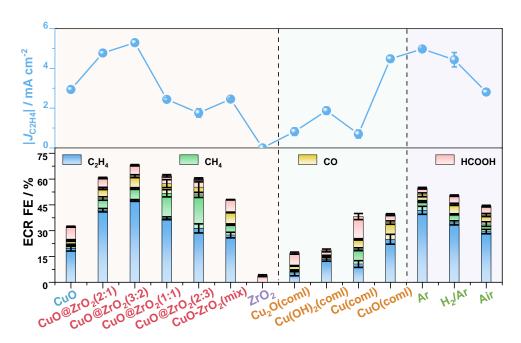


Fig. 4. C₂H₄ partial geometric current density (upper panel) and FE (bottom panel) over CuO@ZrO₂ catalysts with varying Cu/Zr molar ratios, commercial (coml) Cu, Cu₂O, CuO, Cu(OH)₂, treated CuO@ZrO₂ in different atmospheres (Ar, 8% H₂/Ar, and air) at 200 °C for 1 h, and also the pure CuO and ZrO₂ synthesized here at −1.1 V.

We further investigated the impact of Cu⁺ during ECR by annealing CuO@ZrO₂ at 200 °C by exposure to distinct atmospheres (Fig. 4). The relative percentages of Cu⁰, Cu⁺, and Cu²⁺ in the resultant catalysts were analyzed by XPS (Table S2 and Fig. S10). Treatment in Ar to convert a small fraction of Cu²⁺ to Cu⁺ and Cu⁺ to Cu⁰ (Table S2 and Fig. S10a) mildly degraded the ECR activity. The overall ECR FE and C₂H₄ FE as well as partial current density all descended. Annealing the catalyst in 8% H₂/Ar resulted in a more pronounced drop in C₂H₄ FE (to 34.5%). This may be attributed to the lessened Cu⁺/Cu⁰ ratio (Table S2 and Fig. S10b) detrimental to C–C coupling. We also found that treatment of the sample in air at elevated temperatures substantially deteriorated the ECR performance especially the FE for C₂H₄ production, whereas H₂ evolution became more severe. This may be associated with the decrease in Cu⁺/Cu²⁺ (Table S2 and Fig. S10c).

To verify the importance of the CuO–ZrO₂ interface, we mediated the interfacial structure by controlling the feeding sequence of the two metal precursors during synthesis. When Cu(Ac)₂ and ZrCl₄ were added separately to prepare the catalyst, the C₂H₄ FE was markedly reduced (Table S3). In either case, the accessible CuO–ZrO₂ interfaces with exposed copper sites were evidently diminished, thus leading to the declined ECR performance. Alternatively, individual CuO and ZrO₂ were physically mixed as a control (CuO/ZrO₂_mix) that has equivalent metal oxide contents with CuO@ZrO₂, which however gave inferior CO₂ reduction activity (Fig. 4). This is likely owing to the reduced intimate CuO–ZrO₂ interfaces and poor mass transport. Based on the above results, we propose that rational design of CuO–ZrO₂ interfaces to facilitate and stabilize surface Cu⁺ species is vital to accelerate the CO₂-to-C₂H₄ transformation.

Cycling assays with alternated electrolysis between Ar- and CO₂-purged solutions indicated that the C₂H₄ FE remained essentially constant for at least 4 cycles (Fig. 5a). It also supported that the obtained C₂H₄ was generated from the feed gas CO₂. Strikingly, no obvious decay in C₂H₄ current density and FE occurred even following continuous electrolysis for 12 h, reflecting considerable catalytic durability of CuO@ZrO₂ (Fig. 5b). Post characterization by XPS (Fig. S12a and b) manifested that the surface concentration of Cu⁺ was largely maintained after electrolysis at -1.1 V, probably resulting from the strong interplay between ZrO₂ and CuO. In addition, the morphology and size of CuO@ZrO₂ after electrolysis were well preserved, further confirming its good stability (Fig. S11).

We further conducted operando Raman spectroscopy measurements to monitor the catalyst structural evolution in operando during the ECR (Fig. 5c and d). In the spectra measured at the open-circuit potential (OCP), both CuO@ZrO2 and CuO display peaks at 290.6 and 345.2 cm⁻¹ ascribed to CuO. The additional peaks for CuO@ZrO2 at ~380 and 476 cm⁻¹ correspond to ZrO2, whereas the signals at 220.3, 419.0, and 640.1 cm⁻¹ originate from Cu₂O, associated with the respective $2\Gamma_{12}$, $4\Gamma_{12}$, and $\Gamma_{12} + \Gamma_{25}^{+}$ modes.³⁶ Interestingly, the CuO@ZrO2 retains the characteristic Raman modes of Cu₂O within 60 minutes of CO2 electrolysis (Fig. 5c), implying that the ZrO2 can protect Cu⁺ species from further reduction to a great extent. In sharp contrast, for the neat CuO catalyst, the Raman signals of CuO and Cu₂O disappear rapidly after 10 minutes under the realistic operando conditions (Fig. 5d), indicating the full reduction of Cu²⁺ to Cu⁰.

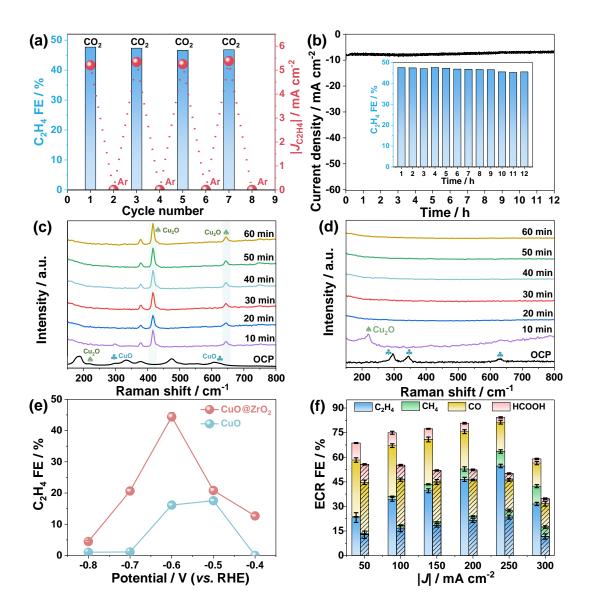


Fig. 5. (a) C₂H₄ FE (bar) and corresponding partial geometric current density (ball) for CuO@ZrO₂ versus alternate cycles with an interval of 1 h in CO₂- and Ar-purged 0.1 M KHCO₃ at −1.1 V. (b) Geometric current density- and C₂H₄ FE (the inset) as a function of electrolysis time on CuO@ZrO₂ for ECR at −1.1 V. Operando Raman spectra of (c) CuO@ZrO₂ and (d) CuO at different ECR reaction times at −1.1 V. (e) FE for C₂H₄ formation via the electrochemical CO reduction over bare CuO and CuO@ZrO₂ in 0.1 M KOH solutions purged with CO at ambient

temperature. (f) ECR FEs of CuO@ZrO₂ and bare CuO over the geometric current range from 50 to 300 mA cm⁻² in a flow cell with 1.0 M aqueous KOH as both catholyte and anolyte.

We found that $CuO@ZrO_2$ also enabled selective electroreduction of CO towards C_2H_4 . The C_2 product started to form at a potential as low as -0.4 V which is rather unlikely for pure CuO. In the entire voltage range between -0.4 and -0.8 V, $CuO@ZrO_2$ showed superior C_2H_4 formation efficiency with the maximum C_2H_4 FE of $44.4 \pm 1.3\%$ at -0.6 V, being 2.5-fold that of pure CuO.

Due to the poor solubility and low diffusion coefficient of CO_2 in aqueous solutions, ECR current densities are usually limited to be less than 30 mA cm⁻² in conventional H-cells. This limitation can be overcome by using a flow reactor which can also shorten the diffusion path for the ECR. Virtually, high current densities exceeding 100 mA cm⁻² were easily achieved in a flow cell with 1.0 M aqueous KOH as the electrolyte. Note that the ECR performance over $CuO@ZrO_2$ invariably surpassed bare CuO. The overall ECR FE is higher than 67.0% throughout the geometric current density regime from 50 to 300 mA cm⁻², approaching 85.4% at 250 mA cm⁻² (Fig. 5f). In particular, at this high current density, an impressive FE of 54.7 \pm 1.1% for C_2H_4 formation was attained, outperforming many previously reported Cu-based electrocatalysts, as presented in Table S4.

Based on the above experiments and analyses, we infer that the presence of ZrO_2 and abundant defects in CuO both favor CO_2 adsorption and activation to yield more *CO formation. Higher *CO coverage facilitates subsequent hydrogenation (to generate COH* or CHO*) and C-C coupling preferably at the sites of Cu^+ on the surface of CuO^{14} . Meanwhile, an oxygen vacancy may also promote rapid desorption of *CH₂, accelerating the conversion of $2*CH_2 \rightarrow C_2H_4$. Among others, the introduction of ZrO_2 effectively suppressed the

undesired HER.^{22,37} The nanopits in CuO may extend the residence time of electrogenerated products (as a result of higher adsorption energy in hole surface than a corresponding planar structure) and/or increase the local pH, thereby improving the C–C coupling probability within the confined space¹⁴.

To gain mechanistic insight into the enhanced C₂H₄ formation on CuO@ZrO₂, we performed DFT modeling (Fig. 6). We calculated the interface between CuO and ZrO₂ by binding a ZrO₂ cluster (Zr₈O₁₆) onto the Cu (111) slab (Fig. 6a and Fig. S13a and b). The variation/trend of the Bader charges on the surface Cu in the presence and absence of ZrO₂ clusters was considered given that the Bader charge qualitatively matches with the oxidation state. It is assumed that the Bader charges of surface Cu in Cu (111), Cu₂O (111), and CuO (111) correlate with the respective oxidation states of 0, +1, and +2. A linear feature between the Bader charge and oxidation state (Fig. 6b) was acquired. The oxidation state of Cu in CuO@ZrO₂ can thus be derived from the correlation. It is obvious that the oxidation states of Cu at the CuO–ZrO₂ interface fall between that of Cu₂O and CuO (Fig. 6b), suggesting that the interfacial ZrO₂ cluster altered the oxidation state of adjacent Cu in CuO towards that of Cu₂O. This matches XPS results (Fig. 1b and c), manifesting the existence of Cu⁺ in CuO@ZrO₂. It can thus be inferred that ZrO₂ plays a central role in stabilizing Cu⁺.

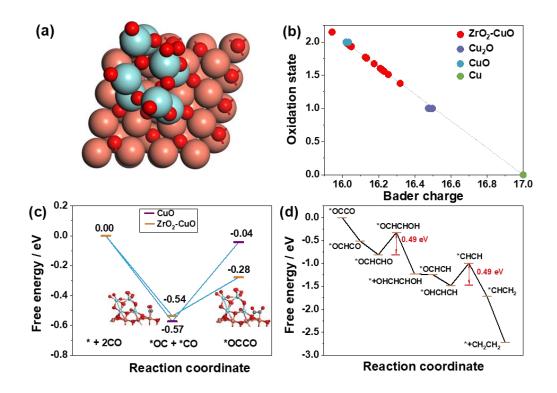


Fig. 6. (a) Top view of the optimized geometries of CuO@ZrO₂. (b) Oxidation states of surface Cu derived by Bader charge investigation. (c) Free energy diagram for *OCCO production starting from * + 2CO over pure CuO and CuO@ZrO₂. (d) Free energy diagram for C₂H₄ production starting from *OCCO over CuO@ZrO₂. All energies are in eV.

We evaluated the capability for C₂ generation by comparison of the energy for dimerization of *CO into *CO dimer (*OCCO), a step that is claimed to be a critical C–C coupling path over copper-based materials. It was calculated that pure CuO and CuO@ZrO₂ both possess a high surface affinity for CO intermediates, which coincides with temperature-programmed desorption of CO (CO-TPD) results (Fig. S14). Note that the dimerization energy of *CO was substantially lowered (from 0.53 to 0.26 eV) for CuO@ZrO₂ compared to pure CuO (Fig. 6c). In addition, the relative energy of *CO + *CO and *OCCO as opposed to * + 2CO (g) is – 0.54 and –0.28 eV, respectively (Fig. 6c). This supports the hypothesis that the incorporation

of ZrO₂ can effectively promote C_2 formation. Fig. 6d reveals the free energy profile for *OCCO to C_2H_4 over $CuO@ZrO_2$ after considering the possible reaction intermediates for C_2 product generation (Fig. S15). The potential determining step is either *OCHCHO + (H⁺ + e⁻) \rightarrow *HCHCHOH or *OHCHCH + (H⁺ + e⁻) \rightarrow *CHCH + H₂O (Fig. 6d). Therefore, at the experimental potential region, $CuO@ZrO_2$ can boost the overall ECR reactions exothermically to yield C_2H_4 .

Our results in this work show that the presence of surface Cu⁺ stabilized by ZrO₂ significantly enhanced ECR to yield C₂H₄. This matches well with many previous reports underpinning the role of Cu⁺ during the ECR.^{17,18,36} However, in some prior literature, ^{13,38,39} surface oxide layer without stabilization was observed fully reduced to metallic Cu before the onset potential and Cu⁰ was proposed as the main active sites for ECR. We envisage that the exact Cu active sites for ECR may be varied dependent on the catalyst systems. Future study using advanced operando spectroscopy measurements in conjunction with ¹³C isotope and rationally designed control experiments by introducing O₂ or O₂/CO₂ mixture would be more helpful to elucidate the specific active sites and reaction pathways.

CONCLUSION

To conclude, we have demonstrated that the introduction of ZrO_2 coupled with tuning of nanocavities in CuO greatly facilitates dimerization and protonation of *CO to yield C_2H_4 for both electrochemical CO_2 and CO reduction reactions. Such a combined strategy also concurrently inhibits the competitive HER. Modulating the content of ZrO_2 incorporation and defects in CuO allows for fine-tuning of the ECR performance. A significantly higher FE of $47.6 \pm 0.5\%$ and cathodic EE of $26.8 \pm 0.3\%$ for C_2H_4 production is achieved over CuO@ZrO₂

in an H-cell, compared to that of only $19.7 \pm 1.5\%$ and $11 \pm 1.9\%$ for bare CuO, respectively. The respective overall FE and FE for C_2H_4 can be further improved up to $84.3 \pm 1.6\%$ and $54.7 \pm 1.1\%$ with a high current density of -250 mA cm⁻² in a flow reactor. Operando Raman spectroscopy and post-XPS measurements confirmed that ZrO_2 can effectively stabilize Cu^+ against further reduction under CO_2 reduction conditions. The activity of the composite catalyst preserves sufficient stability even after continuous polarization over 12 h. DFT analysis reveals the preferred formation of Cu^+ species (which are likely the main sites for CO_2 adsorption and activation) as well as the lower energy barrier for C–C coupling at the CuO– ZrO_2 interface. This work offers a simple and effective scheme for selective electrochemical reduction of CO_2 and CO to produce C_2H_4 .

ASSOCIATED CONTENT

Supporting Information.

The Supporting Information is available free of charge on the ACS Publications website at DOI: Experimental section; XRD; wide-survey, O 1s and Zr 3d XPS spectra; H₂-TPR; SEM and STEM; C₂H₄ partial geometric current density; scan-rate dependence of cyclic voltammetric stripping; Nyquist plots; the FE of ECR products; Cu 2p XPS after electrolysis; SEM and TEM images after electrolysis; the view of the Cu₂O and CuO; CO desorption isotherms; the intermediate of the reduction process of CO₂; summary of C₂H₄ performance over reported electrocatalysts; the relative percentages of Cu⁰, Cu⁺, and Cu²⁺ before and after thermal treatment at different conditions estimated by XPS; the ECR activity optimized by modulating the feeding sequence of the metal salt precursors; summary of C₂H₄ performance over reported electrocatalysts in flow cell.

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Author Contributions

Z. S. supervised the project. Z. S. and X. L. conceived the idea. X. L. conducted synthesis and electrochemical experiments. S. H. and A. W. R. helped transmission electron microscopy measurements and analysis. L. L. performed DFT calculations. Z. S., X. L. and L. L. wrote the manuscript. A. W. R. polished the language. All authors reviewed the manuscript.

Notes

The authors declare no competing financial interest.

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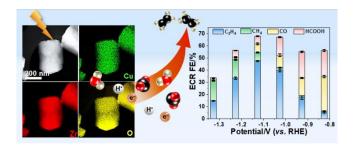
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We demonstrate synergistic electrolysis of CO_2 and CO to C_2H_4 by concurrently tuning nanocavities and the interface of CuO with ZrO_2 .